

Optimization of parameters using response surface methodology and genetic algorithm for biological denitrification of wastewater

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Abstract In the present study the removal of nitrates from wastewater using *Pseudomonas stutzeri* microorganism in a Gas–Liquid–Solid bioreactor at the concentration of 200 ppm was studied for a period of 12 h. The response surface methodology with the help of central composite design and genetic algorithm were employed to optimize the process parameters such as airflow rate, biofilm carrier, carbon source, temperature and pH which are responsible for the removal of nitrates. The optimized values of parameters found from RSM are airflow rate 2.41 lpm, biofilm carrier 15.15 g/L, carbon source 85.0 mg/L, temperature 29.74 °C, pH 7.47 and nitrate removal 193.16. The optimized parameters obtained from genetic algorithm are airflow rate 2.42 lpm, biofilm carrier 15.25 g/L, carbon source 84.98 mg/L, temperature 29.61 °C, pH 7.51 and nitrate removal is 194.14. The value of $R^2 > 0.9831$ obtained for the present mathematical model indicates the high correlation between observed and predicted values. The optimal values for nitrate removal at 200 ppm are suggested according to genetic algorithm and at these optimized parameters more than 96 % of nitrate removal was estimated, which meets the standards for drinking water.

Keywords Central composite design · Gas–Liquid–Solid bioreactor · Nitrate removal · *Pseudomonas stutzeri*

Introduction

Direct discharge of wastewater containing nitrogen can cause environmental problem such as eutrophication of rivers and serious health problems in humans such as the blue baby syndrome in infants, liver damage and cancer (Gupta et al. 2003; Shrimali and Singh 2001). Extractive methods like reverse osmosis, electro-dialysis and ion exchange resins (Choi and Batchelor 2008; Schoeman and Steyn 2001; Park et al. 2008) produce a large amount of effluent containing high concentration of nitrate, which results in the second pollution, which must be treated later and thus increasing the overall cost of the process.

Biological denitrification has been focused by a large number of researchers recently (Rezaee et al. 2008; Kim et al. 2005; Foglar et al. 2005; Roanders and Xin-Min 2004; Wen et al. 2003; Hirata et al. 2001; Soares 2000), and work reported on biological denitrification of wastewater using a fluidized bed bioreactor is very little using *Pseudomonas stutzeri*. Biological treatment has high treatment efficiency, no sludge production, small area occupied and relatively low investment costs.

Biological denitrification occurs naturally when certain bacteria use nitrate as terminal electron acceptor in their respiratory process, in the absence of oxygen. Denitrification consists of a sequence of enzymatic reactions leading to the evolution of nitrogen gas. The process involves the formation of a number of nitrogen intermediates and in these processes microorganisms first reduce nitrates to nitrites and then produce nitric oxide, nitrous oxide and nitrogen gas. The pathway for nitrate reduction is:



Biological denitrification treatment consists of the provision of suitable carbon sources, which may be organic or

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inorganic compounds. Several sources of carbon with different combinations have been used for denitrification including succinic acid, ethanol and acetic acid (Kesseru et al. 2002), acetate, ethanol and hydrolysed rice (Khanithachaidecha et al. 2010), methanol (Ginige et al. 2009), news paper, cotton (Volokita et al. 1996a, b), acetate, ethanol and methanol (Adav et al. 2010), rice husk (Shao et al. 2008) and molasses (Ueda et al. 2006). Based on its price and availability, methanol is most commonly used as additional carbon source for bacterial denitrification. The combinations of parameters like airflow rate, biofilm carrier, carbon source, temperature and pH have not been studied by earlier investigators; these combinations are employed in the present experiments varying at different levels.

The response surface methodology (RSM), which is an efficient statistical technique for optimization of multiple parameters with minimum number of experiments, is to use a set of designed experiments to obtain an optimal response (Li et al. 2010; Vohra and Satyanarayana 2002; Francis et al. 2003). This technique has been applied in a wide range of fields such as drug and food industry, chemical and biological processes (Meilgaard et al. 1991; Otto 1999). RSM has been successfully applied to different processes for optimization of the experimental design. However, to our best knowledge, the application in biological reduction of nitrate removal (NR) with above said parameters is not yet reported.

The objective of the current study is to optimize the parameters like airflow rate, biofilm carrier, carbon source, temperature and pH at different levels using RSM and genetic algorithm (GA) for a initial nitrate concentration of 200 ppm using *P. stutzeri* microorganism in Gas–Liquid–Solid bioreactor (GLS).

Research work was carried out during January to April 2012 at Department of Chemical Engineering, National Institute of Technology, Warangal, Andhra Pradesh, India.

Materials and methods

Cell immobilization and inoculation of denitrifying bacteria

The experimental work was carried out in a GLS with attached growth process to investigate the removal of nitrate from the synthetic wastewater and *P. stutzeri* with low density polymer (polypropylene) used as the supporting media. The bacterium from the slants was inoculated into liquid broth containing nitrate concentration of 200 mg/L and was prepared by mixing: 48.9 mg of KNO_3 , 6 mg of $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 0.2 mg of $\text{FeCl}_3 \cdot 7\text{H}_2\text{O}$, 430 mg of Na_2HPO_4 and 320 mg of $\text{Na}_2\text{H}_2\text{PO}_4$ (Lakshmi and Pydi

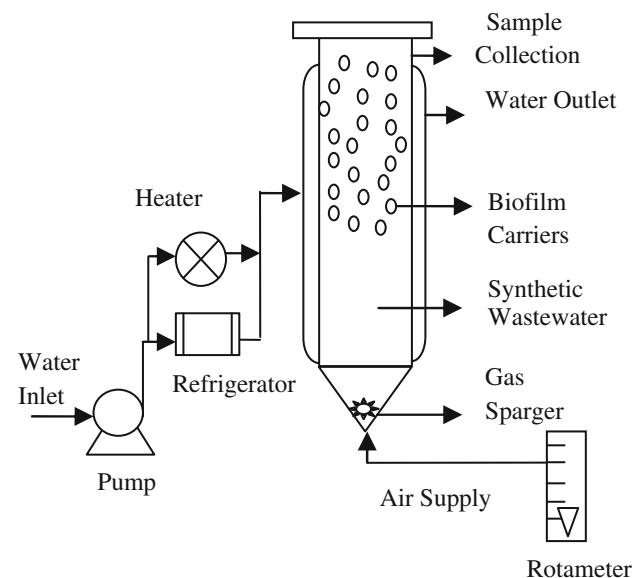


Fig. 1 Gas–Liquid–Solid bioreactor

2008). The composition gives the initial nitrate concentration of 30 mg/L, to increase or decrease the nitrate composition we can vary the amount of potassium nitrate proportionately.

Experimental set-up

The GLS consists of a glass column of 0.5 m height, 93 mm of internal diameter (ID) and 100 mm of outer diameter (OD) with a capacity of 3.4 L. The setup was provided with a glass jacket of 118 mm ID and 122 mm OD, to maintain the temperature of the reactor and also provision was made for the supply of air/ N_2/O_2 based on the requirement. A gas sparger was located at the base of column for uniform distribution of gas as shown in Fig. 1.

Analytical methods

All the analysis was done according to standard methods (APHA 2005). Runs were conducted according the central composite design (CCD) combinations and samples was collected for every 1 h, filtered and were used for the

Table 1 Different factors used in the experiment and their levels

Parameters	Coding	Levels	
		Low	High
Airflow rate (lpm)	AF	2	3
Biofilm carriers (g/L)	BC	10	20
Carbon source (mg/L)	CS	75	85
Temperature (°C)	Temp	25	35
pH	pH	6	8

Table 2 Planning matrix of the experiments according to CCD in actual level of variables and predicted and observed response functions for optimization of process parameters for nitrate removal

Std	Run	AF	BC	CS	Temp	pH	Response NR (actual value)	Predicted value	Residual
1	31	2	10	75	25	6	172	172.28	-0.28
2	1	3	10	75	25	6	174	172.28	1.72
3	10	2	20	75	25	6	176	176.11	-0.11
4	33	3	20	75	25	6	173	173.74	-0.74
5	34	2	10	85	25	6	174	174.62	-0.62
6	41	3	10	85	25	6	174	174	E-003
7	15	2	20	85	25	6	180	179.84	0.16
8	35	3	20	85	25	6	176	176.84	-0.84
9	38	2	10	75	35	6	170	170.56	-0.56
10	24	3	10	75	35	6	172	171.18	0.82
11	45	2	20	75	35	6	173	172.52	0.48
12	23	3	20	75	35	6	170	170.77	-0.77
13	25	2	10	85	35	6	175	174.78	0.22
14	40	3	10	85	35	6	174	174.78	-0.78
15	11	2	20	85	35	6	178	178.11	-0.11
16	30	3	20	85	35	6	176	175.74	0.26
17	39	2	10	75	25	8	177	176.62	0.38
18	37	3	10	75	25	8	176	177	-1
19	50	2	20	75	25	8	175	176.84	-1.84
20	42	3	20	75	25	8	178	174.84	3.16
21	27	2	10	85	25	8	184	182.59	1.41
22	43	3	10	85	25	8	182	182.34	-0.34
23	28	2	20	85	25	8	185	184.18	0.82
24	48	3	20	85	25	8	180	181.56	-1.56
25	49	2	10	75	35	8	178	174.78	3.22
26	20	3	10	75	35	8	174	175.78	-1.78
27	26	2	20	75	35	8	173	173.11	-0.11
28	18	3	20	75	35	8	172	171.74	0.26
29	5	2	10	85	35	8	180	182.62	-2.62
30	7	3	10	85	35	8	186	183	3
31	21	2	20	85	35	8	182	182.34	-0.34
32	19	3	20	85	35	8	180	180.34	-0.34
33	4	2	15	80	30	7	188	188.11	-0.11
34	13	3	15	80	30	7	186	187.11	-1.11
35	46	2.5	10	80	30	7	181	183.82	-2.82
36	9	2.5	20	80	30	7	186	184.4	1.6
37	47	2.5	15	75	30	7	184	186.88	-2.88
38	2	2.5	15	85	30	7	194	192.35	1.65
39	12	2.5	15	80	25	7	187	187.35	-0.35
40	29	2.5	15	80	35	7	185	185.88	-0.88
41	44	2.5	15	80	30	6	185	183.88	1.12
42	17	2.5	15	80	30	8	186	188.35	-2.35
43	14	2.5	15	80	30	7	190	189.39	0.61
44	3	2.5	15	80	30	7	190	189.39	0.61
45	32	2.5	15	80	30	7	190	189.39	0.61
46	22	2.5	15	80	30	7	190	189.39	0.61
47	6	2.5	15	80	30	7	190	189.39	0.61



Table 2 continued

Std	Run	AF	BC	CS	Temp	pH	Response NR (actual value)	Predicted value	Residual
48	8	2.5	15	80	30	7	190	189.39	0.61
49	16	2.5	15	80	30	7	190	189.39	0.61
50	36	2.5	15	80	30	7	190	189.39	0.61

analysis of final nitrate concentration using Orion ion potentiometer.

Response surface methodology

Response surface methodology is a collection of mathematical and statistical techniques that are useful for modeling and analysis of problems in which output or response influenced by several factors and the goal is to find the correlation between the response and the factors (Parimala et al. 2011). It is also used for optimizing the response at different levels (Montgomery 1990; Raissi and Eslami 2009). The CCD is used since it gives a comparatively accurate prediction of all response variable averages related to quantities measured during experimentation (Theodore 2006). In this method, there is a possibility that the experiments will stop with fairly few runs and decide that the prediction model is satisfactory. In this study, we selected five experimental factors capable of influencing the NR efficiency at 200 ppm and those are shown in Table 1.

The optimization of parameters was conducted using CCD. The response function of interest is NR. These functions were approximated by a second degree polynomial of cubic, quadratic and interaction effects using the method of least squares. There was a set of total 50 experiments generated using CCD design with 43 being the combinations of the actual level of the experimental variables while the remaining 7 were replications at the central points, the experiments were conducted according to CCD and presented in Table 2.

Genetic algorithm

Genetic algorithm is a stochastic global search and optimization method that mimic the metaphor of natural biological evolution. GA operates on a population of potential solutions, applying the principle of survival of the fittest to produce successively better approximations to a solution. At each generation of a GA, a new set of approximations is created by the process of selecting individuals according to their level of fitness in the problem domain and reproducing them using operators borrowed from natural genetics. This process leads to the evolution of populations

Table 3 ANOVA test for response function nitrate removal (NR)

Source	Sum of squares	df	Mean square	F value	p value	prob > F
Model	2113.71	20	105.69	34.03	<0.0001	significant
<i>A-AF</i>	8.50	1	8.50	2.74	0.1088	
<i>B-BC</i>	2.94	1	2.94	0.95	0.3385	
<i>C-CS</i>	254.38	1	254.38	81.90	<0.0001	
<i>D-Temp</i>	18.38	1	18.38	5.92	0.0214	
<i>E-pH</i>	169.88	1	169.88	54.70	<0.0001	
<i>AB</i>	11.28	1	11.28	3.63	0.0666	
<i>AC</i>	0.78	1	0.78	0.25	0.6198	
<i>AD</i>	0.78	1	0.78	0.25	0.6198	
<i>AE</i>	0.28	1	0.28	0.091	0.7656	
<i>BC</i>	3.78	1	3.78	1.22	0.2789	
<i>BD</i>	7.03	1	7.03	2.26	0.1432	
<i>BE</i>	26.28	1	26.28	8.46	0.0069	
<i>CD</i>	7.03	1	7.03	2.26	0.1432	
<i>CE</i>	28	1	26.28	8.46	0.0069	
<i>DE</i>	0.031	1	0.031	0.010	0.9208	
<i>A²</i>	7.83	1	7.83	2.52	0.1232	
<i>B²</i>	68.93	1	68.93	22.20	<0.0001	
<i>C²</i>	0.12	1	0.12	0.039	0.8452	
<i>D²</i>	19.11	1	19.11	6.15	0.0192	
<i>E²</i>	26.60	1	26.60	8.56	0.0066	
Residual	90.07	29	3.11			
<i>Lack of fit</i>	90.07	22	4.09			
<i>Pure error</i>	0.000	7	0.000			
Cor Total	2203.78	49				

$R^2 = 0.9831$, Adj. $R^2 = 0.9409$, Pred. $R^2 = 0.9494$

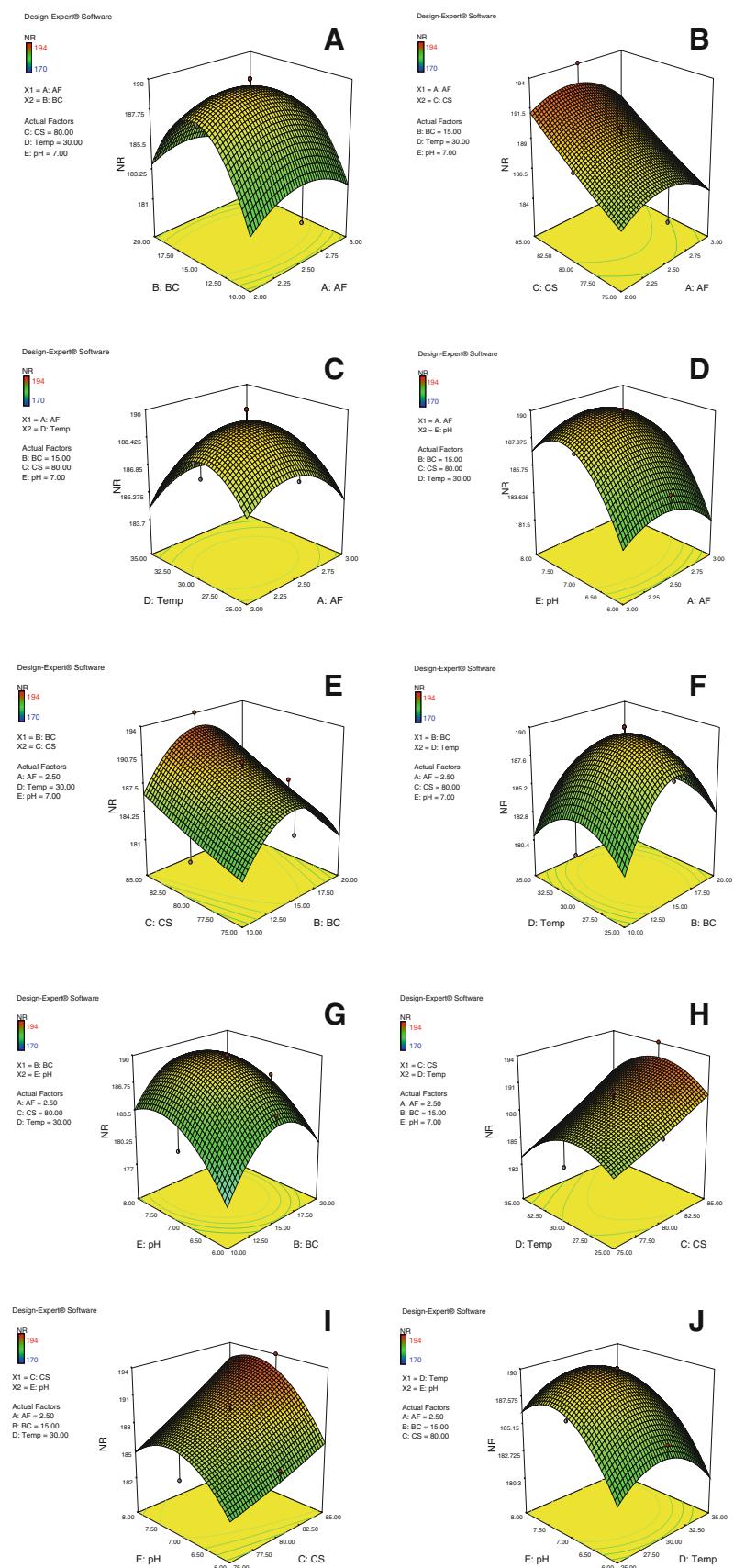
of individuals that are better suited to their environment than the individuals from which they were created, just as in natural adaptation.

Results and discussion

The CCD was used to find the optimal parameter for the NR from wastewater using *P. stutzeri* microorganism. The results of CCD experiments consisted of predicted and experimental data for studying the effects of five independent variables; viz., airflow rate, biofilm carrier, carbon



Fig. 2 Response surfaces plots showing the mutual effect of biofilm carriers and airflow rate (a), carbon source and airflow rate (b), temperature and airflow rate (c), pH and airflow rate (d), carbon source and biofilm carriers (e), temperature and biofilm carriers (f), pH and biofilm carriers (g), temperature and carbon source (h), pH and carbon source (i), pH and temperature (j), for nitrate removal



source, temperature and pH for denitrification are presented in Table 2.

The regression equation obtained from analysis of variance (ANOVA) indicated that the multiple correlation coefficient of R^2 is 0.9831, i.e. the model can explain 98.31 % variation in the response. It should be noted that a R^2 value greater than 0.75 indicates the aptness of the model. The adjusted R^2 and predicted R^2 values are 0.9409 and 0.9494, respectively. ANOVA results confirmed a satisfactory adjustment of the simplified quadratic model to the experimental data. It should be considered that the

polynomial model is a reasonable approximation of the true functional relationship on a relative small region of the entire space of the independent values. The data were fitted with a second-order polynomial function. The ANOVA is shown in Table 3. The simplified second-order polynomial equation for NR in terms of actual factors is expressed as follows: $NR = -39.45283 + 39.96121 \times AF + 7.71900 \times BC - 2.74660 \times CS + 5.19204 \times Temp + 36.08314 \times pH - 0.23750 \times AF \times BC - 0.062500 \times AF \times CS + 0.062500 \times AF \times Temp + 0.18750 \times AF \times pH + 0.013750 \times BC \times CS - 0.018750 \times BC \times Temp$

Fig. 3 Optimized parameter with the help of RSM

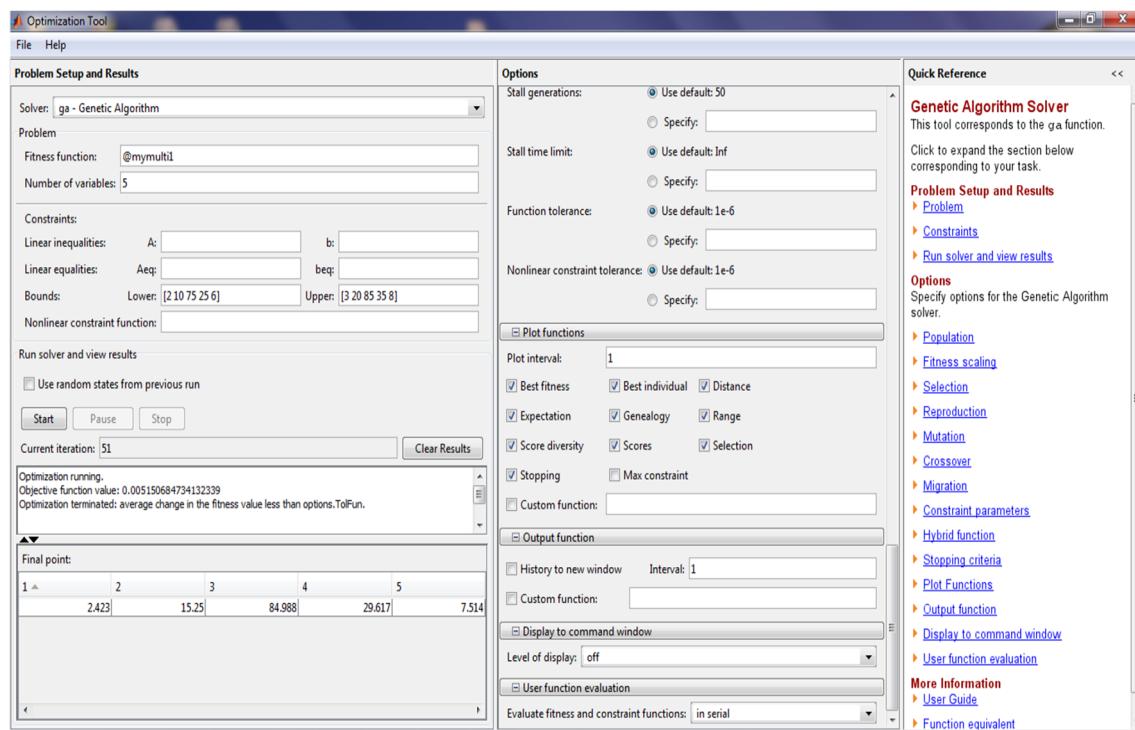
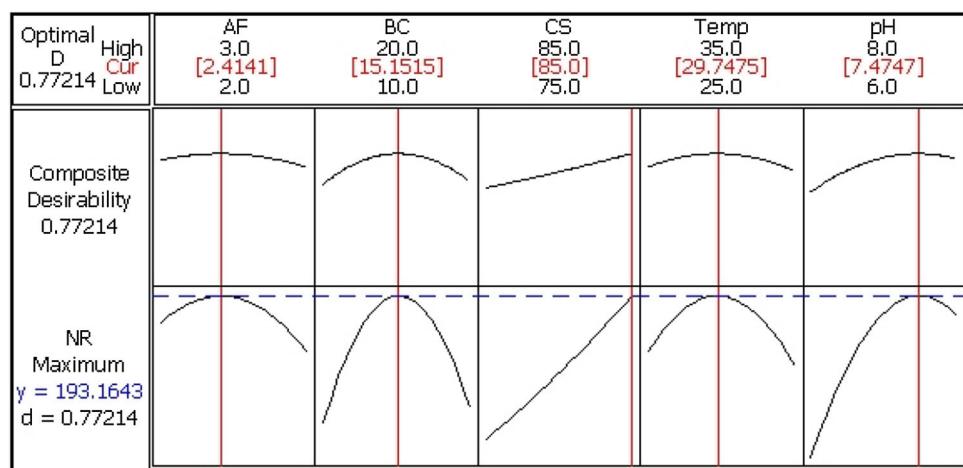


Fig. 4 Screen print of GA which indicates the optimized parameters for denitrification



Table 4 Optimum parameters according to RSM and genetic algorithm

Factors	RSM	Response NR (ppm)	GA	Response (NR)
Airflow rate (lpm)	2.4141		2.423	
Biofilm carrier (g/L)	15.1515		15.25	
Carbon source (mg/L)	85.0	193.1643	84.988	194.149
Temperature (°C)	29.7475		29.617	
pH	7.4747		7.514	

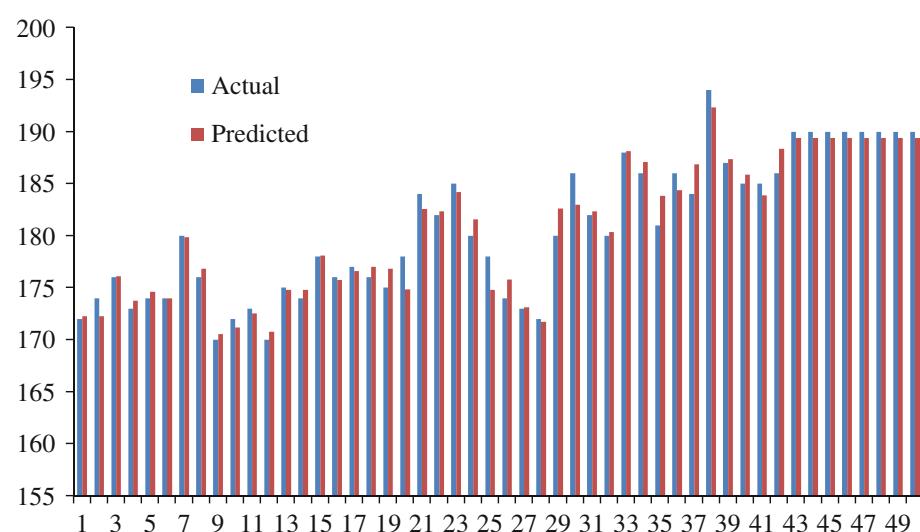
$$-0.18125 \times BC \times pH + 0.018750 \times CS \times Temp + 0.18125 \times CS \times pH - 6.25000E - 003 \times Temp \times pH - 7.11724 \times AF2 - 0.21117 \times BC^2 + 8.82759E - 003 \times CS^2 - 0.11117 \times Temp^2 - 3.27931 \times pH^2.$$

Mutual effects of parameters on NR

Figure 2 represents the mutual effect on NR. The highest denitrification efficiency was obtained at airflow rate ranging from 2 to 3 lpm, biofilm carrier ranging from 10 to 20 g/L, carbon source ranging from 75 to 85 mg/L, temperature ranging from 25 to 35 °C and pH ranging from 6 to 8. The response surface plots of mutual effects of airflow rate, biofilm carriers, carbon source, temperature and pH on NR are shown in Fig. 1(a–j).

The results indicate that highest NR was obtained when airflow rate is at 2.4 lpm, biofilm carrier is 15 g/L, carbon source maintained at 85 mg/L, temperature 30 °C and pH at 7. From the experiments, it is confirmed that the NR efficiency for the said parameters levels could be achieved more than 96 %.

The maximum NR can also be obtained from the following multi interaction combinations by keeping other parameters constant at optimum levels.

Fig. 5 Observation of predicted and actual values

1. Interaction between biofilm carriers and airflow rate (Fig. 1a): 15 g/L and 2.75 lpm.
2. Interaction between carbon source and airflow rate (Fig. 1b): 85 mg/L and 2 lpm.
3. Interaction between temperature and airflow rate (Fig. 1c): 27 °C and 2.5 lpm.
4. Interaction between pH and airflow rate (Fig. 1d): 7 and 2.75 lpm.
5. Interaction between carbon source and biofilm carriers (Fig. 1e): 85 mg/L and 15 g/L.
6. Interaction between temperature and biofilm carriers (Fig. 1f): 30 °C and 17.50 g/L.
7. Interaction between pH and biofilm carriers (Fig. 1g): 7 and 17.50 g/L.
8. Interaction between temperature and carbon source (Fig. 1h): 30 °C and 85 mg/L.
9. Interaction between pH and carbon source (Fig. 1i): 7 and 86 mg/L.
10. Interaction between pH and temperature (Fig. 1j): 7.50 and 32.50 °C.

Figures 3 and 4 represents the optimal parameters for biological denitrification wastewater at the initial nitrate concentration of 200 ppm and operated for a period of 12 h. And it was observed that more than 193.1643 ppm of nitrates were removed with the optimized combination of parameters using RSM and 194.149 ppm removed with the combination of GAs. Optimal parameters and NR for both methods were shown in Table 4. Figure 5 shows the comparison between predicted and actual values.

Conclusion

Biological denitrification of wastewater was studied in a GLS using *P. stutzeri* microorganism at 200 ppm for a



period of 12 h. The optimization of process parameters for denitrification was studied with RSM and GA. The parameters were studied at low and high range of airflow rate: 2–3 lpm, biofilm carrier: 10–20 g/L, carbon source: 75–85 mg/L, temperature: 25–35 °C and pH 6–8. The optimized values of parameters found using RSM is airflow rate 2.41 lpm, biofilm carrier 15.15 g/L, carbon source 85.0 mg/L, temperature 29.74 °C, pH 7.47 and NR is 193.16. The optimized parameters according to GA are airflow rate 2.42 lpm, biofilm carrier 15.25 g/L, carbon source 84.98 mg/L, temperature 29.61 °C, pH 7.51 and NR is 194.14.

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